



Whatever Happened to Pump Stroke Optimization?

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ENCLINE



History of Pump Stroke Optimization

- ▶ Concept and data from two pilot wells first presented to industry at ALRDC Sucker Rod Pumping Workshop in September 2015
- ▶ Case Study of 20 Well Eagle Ford pilot presented at Southwestern Petroleum Short Course in April 2016, and in peer reviewed SPE Paper 181228-PA
- ▶ Four well Bakken pilot presented in September 2016 at ALRDC Sucker Rod Pumping Workshop



What is Pump Stroke Optimization?

- ▶ Part 1: For wells with excess pump capacity, preferentially slowing pumping speed on downstroke
 - ▶ Results in less slippage and better pump fillage
 - ▶ Referred to as Slow Downstroke Mode or SDSM
- ▶ Part 2: Address the problem of wave and slug flow in horizontal wells that mislead RPC's into cycling between max and min speeds
 - ▶ Results in poor pump fillage and rod buckling
 - ▶ Requires setting max pumping speed near average



PSO Part 1: “Slow Downstroke Mode”

Two ways to run at 3 SPM

- ▶ Old School Method for 3 SPM
 - ▶ Total stroke duration is 20 seconds
 - ▶ Upstroke duration is 10 seconds, as is downstroke
- ▶ Slow Downstroke Mode (SDSM)
 - ▶ 6 SPM on upstroke, a 5 second duration
 - ▶ 2 SPM on downstroke, a 15 second duration
 - ▶ Total stroke duration still 20 seconds but upstroke duration only 25% of each stroke, not 50% (5/20 instead of 10/20)

SDSM Example: Pumping at 3 SPM

Artificial Lift
R&D Council



2015 Sucker Rod Pumping Workshop

Use of the Pump Slippage Equation to Design Pump Clearances (Rowlan, McCoy, Lea)

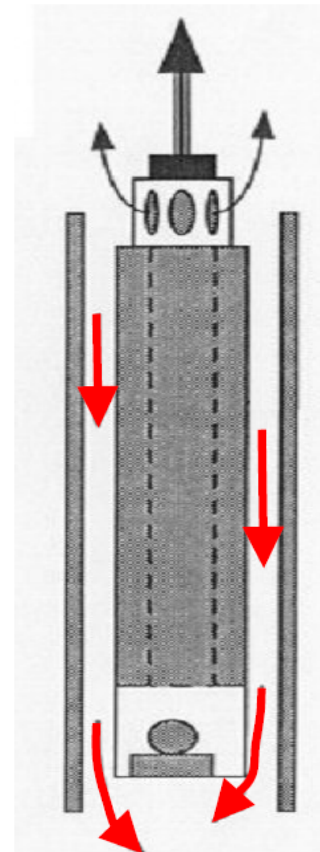
Pump Slippage

- 1) Fluid that leaks back into pump between the Plunger OD and the Barrel ID
- 2) Leaks into the pump chamber between the standing valve and traveling valve
- 3) When traveling ball is on Seat.

Pump Efficiency =
 $\text{BPD Tank} / \text{BPD Pump}$

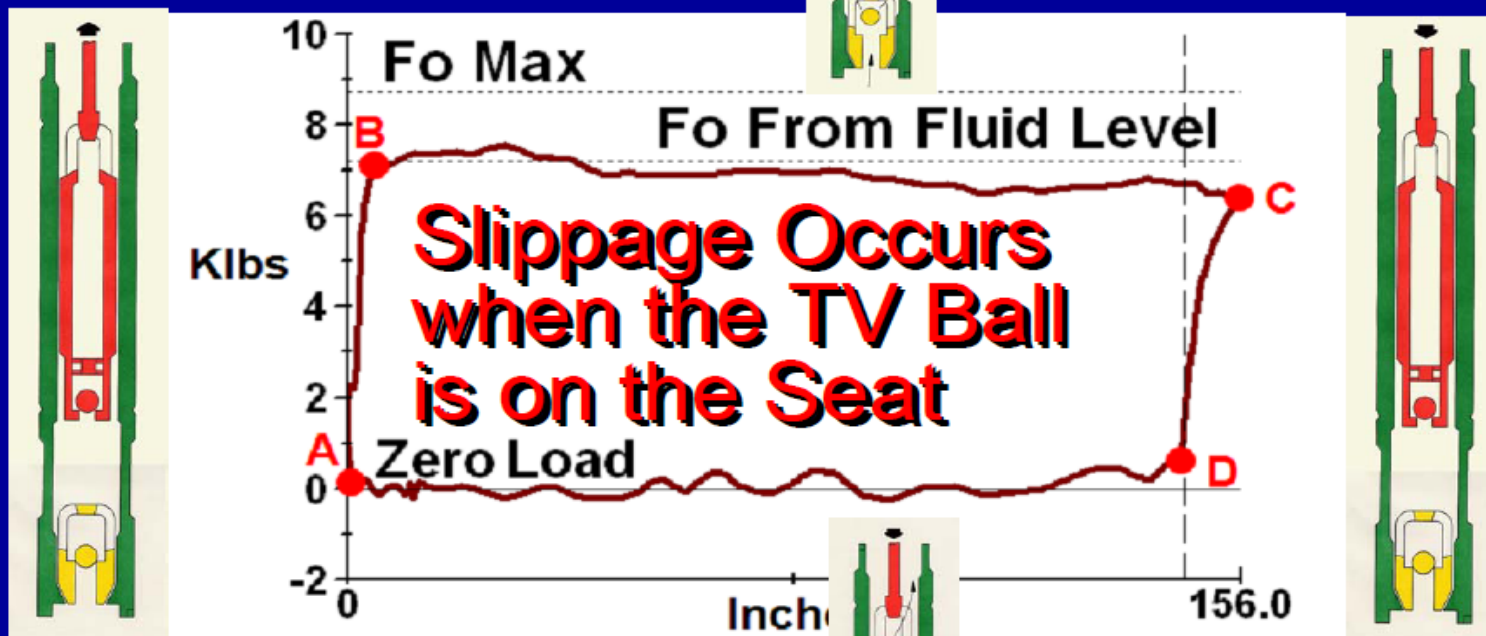
Slippage % =
 $\text{Slippage BPD} / \text{BPD Pump}$

BPD Tank = BPD Pump
- **Slippage**



1) Point A to B pressure acting on closed SV gradually transferred from tubing at point A to be fully carried by the Closed TV at point B.

2. Point B to C, plunger carries full differential pressure across Closed TV



4) Point D to A, TV open as fluid in the pump is displaced through the traveling valve on the down stroke

3) Point C to D pressure across closed TV gradually transferred from rods to be fully carried by the Closed SV at point D.

Observations about Pump Slippage



- ▶ Pump Slippage during the Upstroke reduces system efficiency
 - ▶ Since standing valve is open, slippage replaces fluid that would normally enter pump
 - ▶ Less Time on Upstroke = Less pump slippage
- ▶ Pump slippage during the Downstroke does not impact system efficiency, but improves fillage
 - ▶ Since standing valve closed during downstroke, new well fluids not entering the pump anyway
 - ▶ Slippage fluids fill pump, opening travelling valve sooner
 - ▶ Pump fillage increased, reduced rod buckling

From SPE 181228: Pump Slippage Equation Correction



- ▶ 2001 Thesis by Chambliss submitted to Texas Tech: “Plunger Leakage and Viscous Drag for Beam Pump Systems”
 - ▶ Pump slippage greater for alternative geometry pumping units that had unequal upstroke and downstroke travel time

$$B_{Adjusted} = \frac{Degrees_{UP}}{180} B_{Calculated}$$

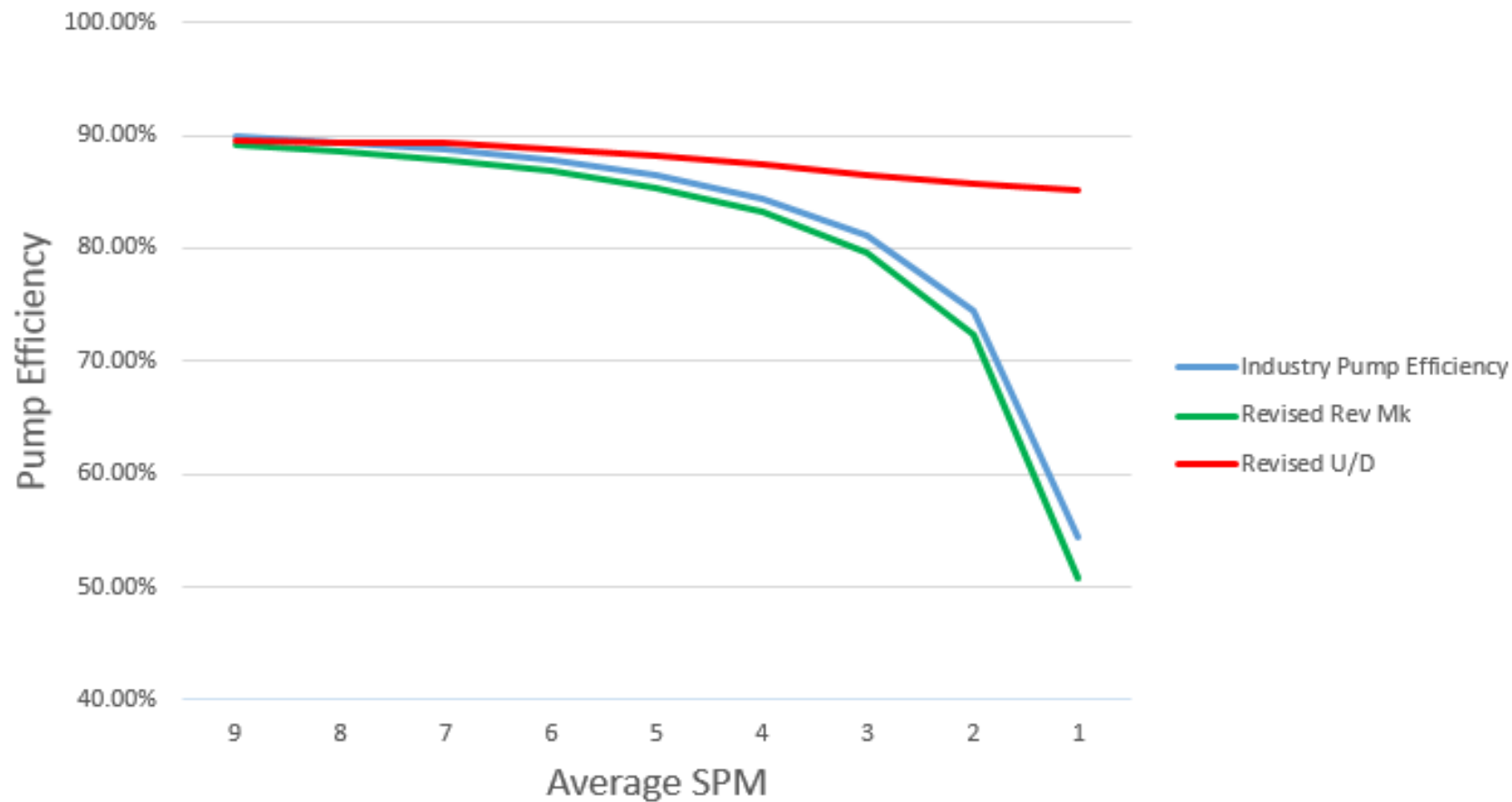
- ▶ However, Chambliss did not consider variation in pumping speed induced travel time differences. A revised equation that considers both is presented:

$$B_{Adjusted} = (2 \times T_{Upstroke} \times B_{Calculated}) / (T_{Downstroke} + T_{Upstroke})$$

Patterson slippage formula modified for % Upstroke Duration



Pump Efficiency Using Arco-HF-COP
Base, Reverse Mark, U/D Speed Control
1.5" Pump at 10000 Feet with .006 clearance, 0.7 vis
350 psi PIP, 6 foot plunger, 0.8 gravity fluid
4 SPM Max SPM Differential, 4 sec Accel/Decel



PSO Part Two: Setting Pumping Speeds





How do operators address poor pump fillage due to horizontal well slugging?

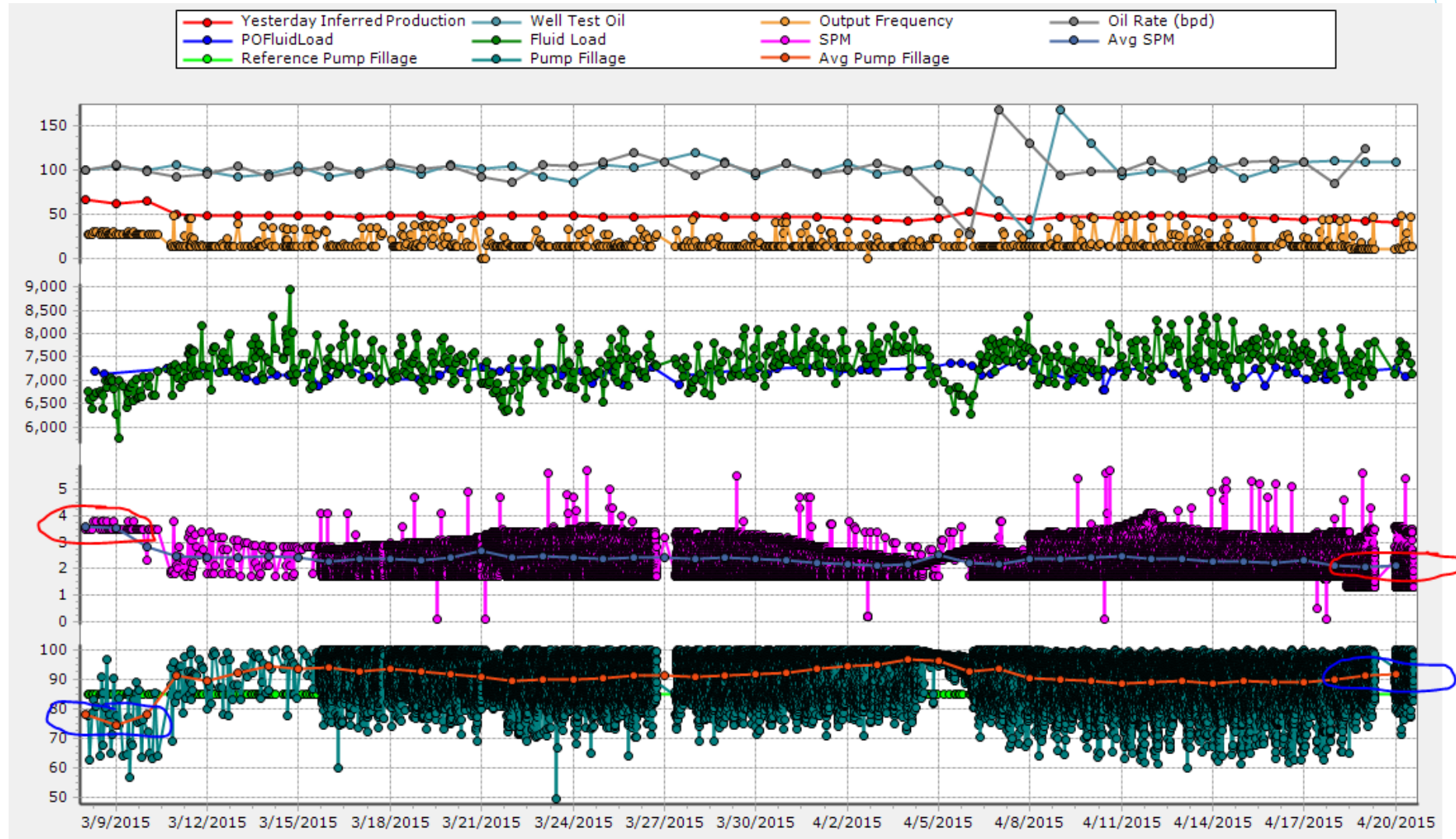
- ▶ By manually setting pumping speed
 - ▶ Limiting maximum pumping speed
 - ▶ Reducing the minimum pumping speed
- ▶ The current approach requires
 - ▶ Regular monitoring by personnel
 - ▶ Resetting pumping speeds as wells continue to deplete
- ▶ PSO Part 2 is autonomous setting of these speeds



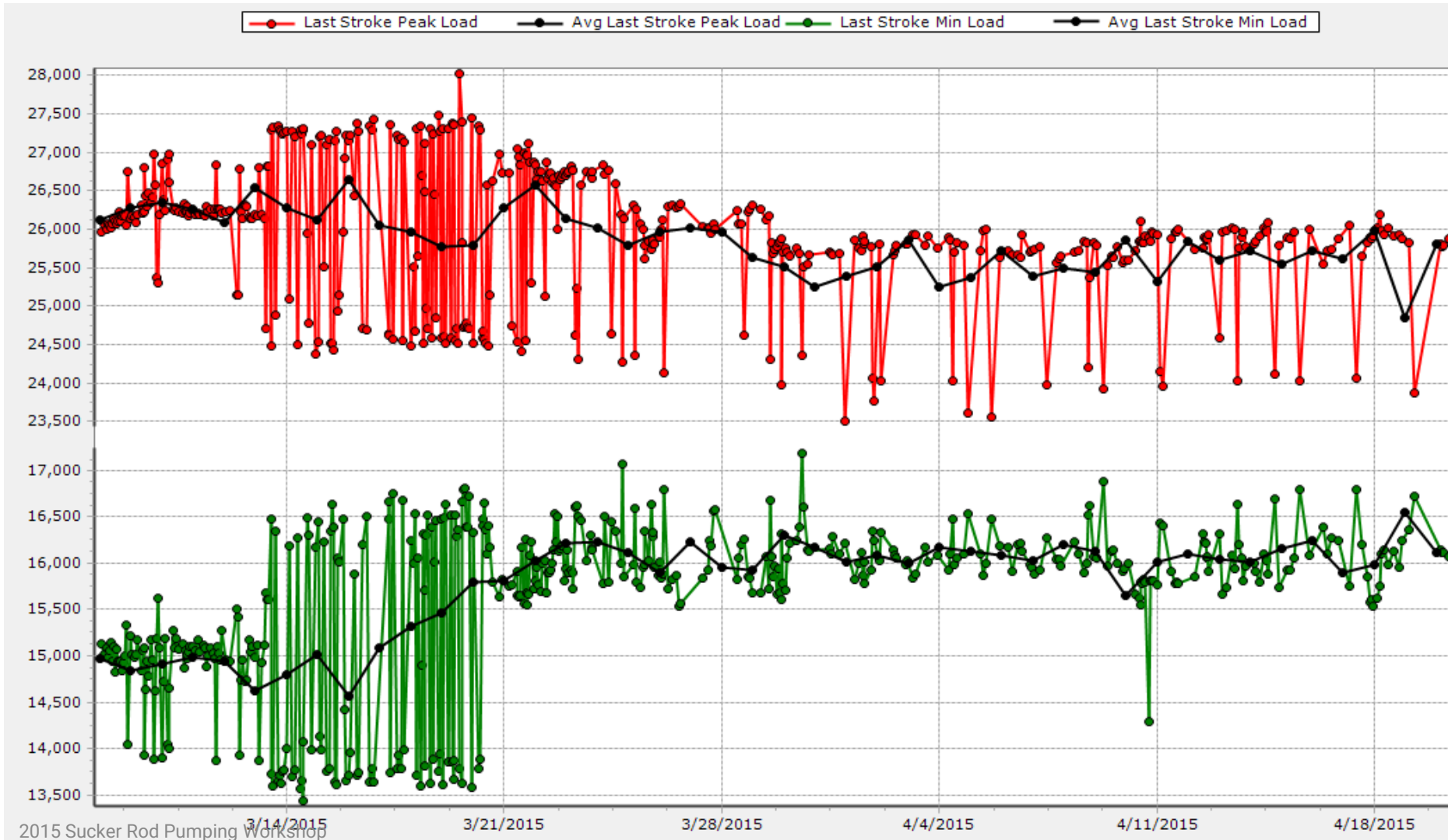
SDSM (PSO Part 1) decreases slippage and increases pump fillage, increasing efficiency

- ▶ Also more time for evolving gas to exit gas anchor
 - ▶ Less gas enters pump, more liquid
- ▶ Higher minimum rod loads due to slow downstroke/ less gas
 - ▶ Reduces buckling tendencies
 - ▶ Allows higher maximum rod loads
- ▶ **Has nothing to do with setting pumping speeds**
 - ▶ That is PSO Part 2

Well #1: 35% reduction in strokes per day, oil production not significantly affected



Well #1: Minimum load increased by 1000 pounds, maximum load same





Why PSO Part 2 works

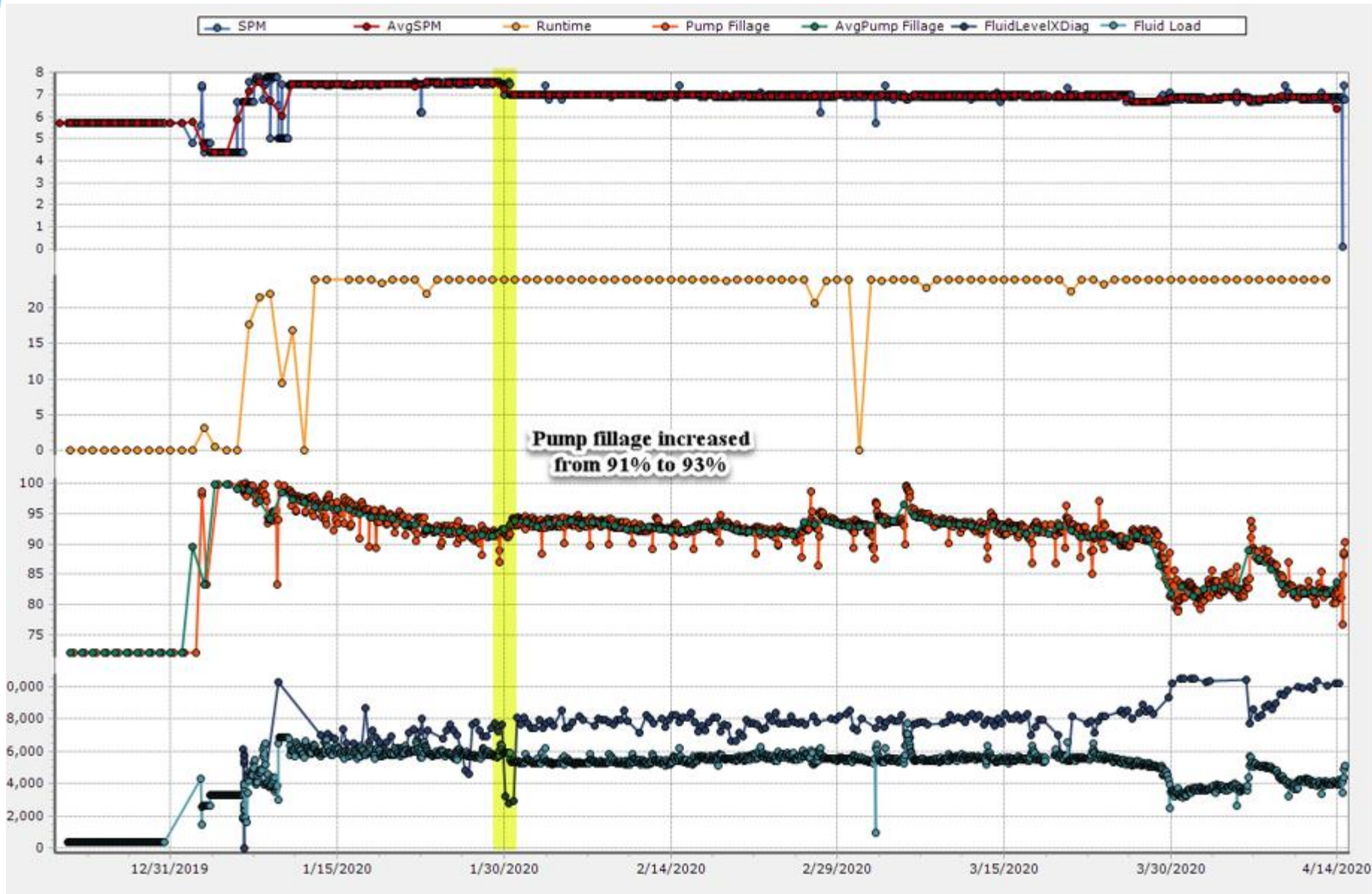
- ▶ PSO Part 2 does what you would do, create maximum working speed setpoints that are better aligned with the average production rate
- ▶ This prevents over-reacting to high pump fillages often seen at the beginning of a slug event
- ▶ Keeping the maximum pumping speed slightly higher than average pumping speed helps avoid low pump fillage events and rod buckling

Some operators are using SDSM today

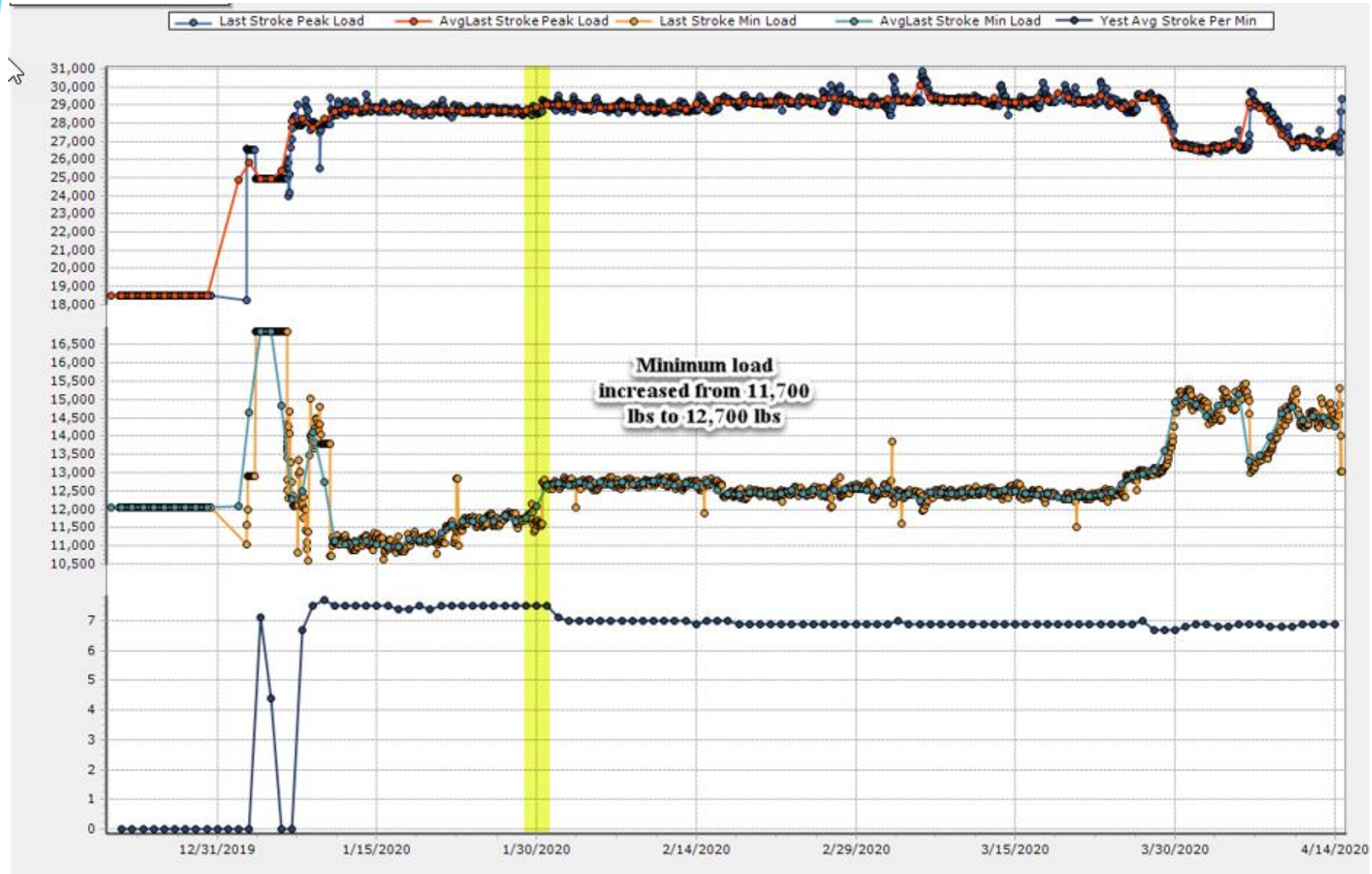


- ▶ Continental Resources using SDSM in Bakken
 - ▶ No hardware modifications needed
 - ▶ Using Scada to load SDSM settings into RPC's
- ▶ EOG Resources using SDSM in Eagle Ford
 - ▶ Working towards applying PSO Part 2 via Data Analytics

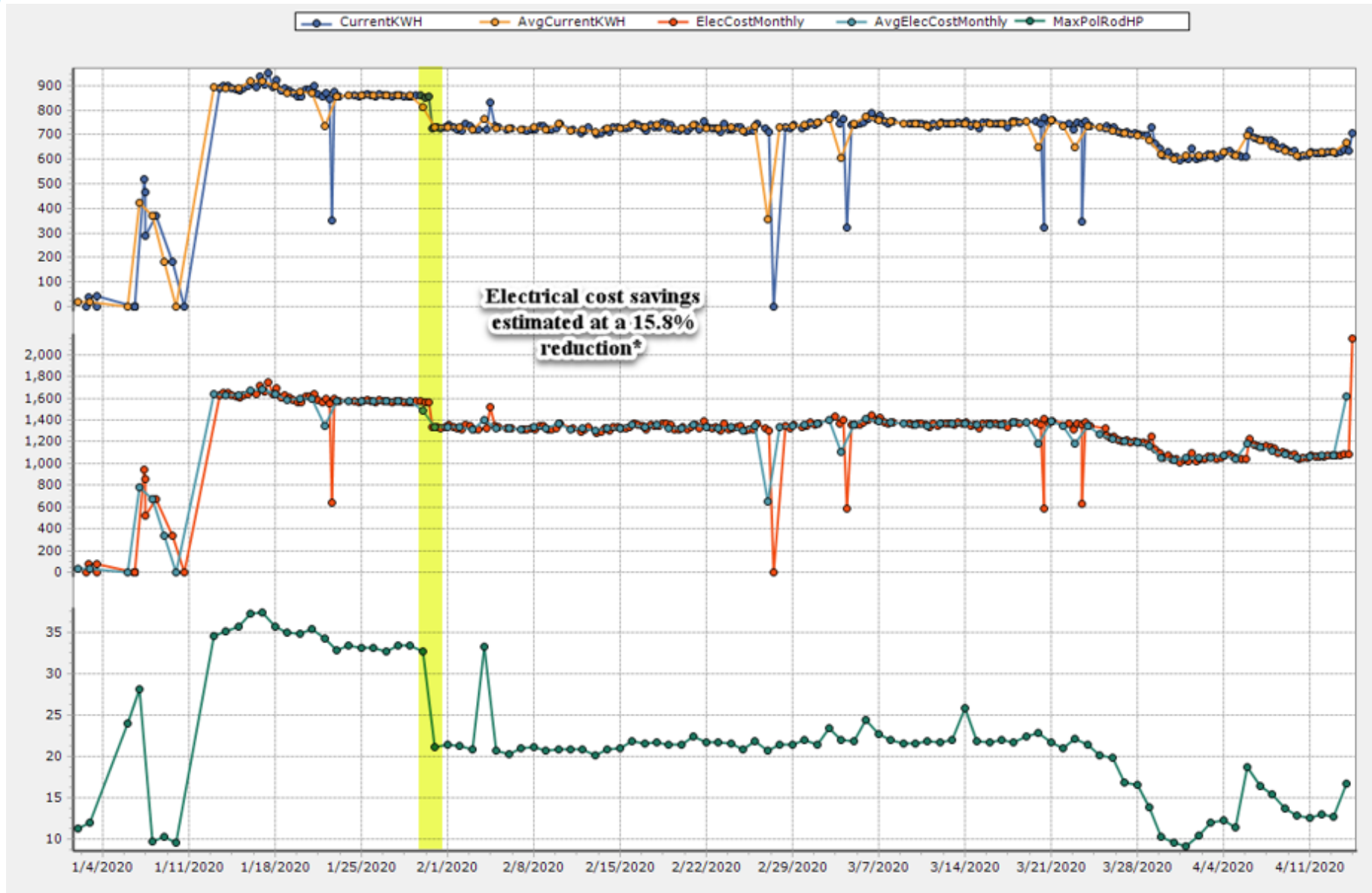
Continental Resources SDSM Results



Continental Resources SDSM Results



Continental Resources SDSM Results



Continental Resources SDSM Results



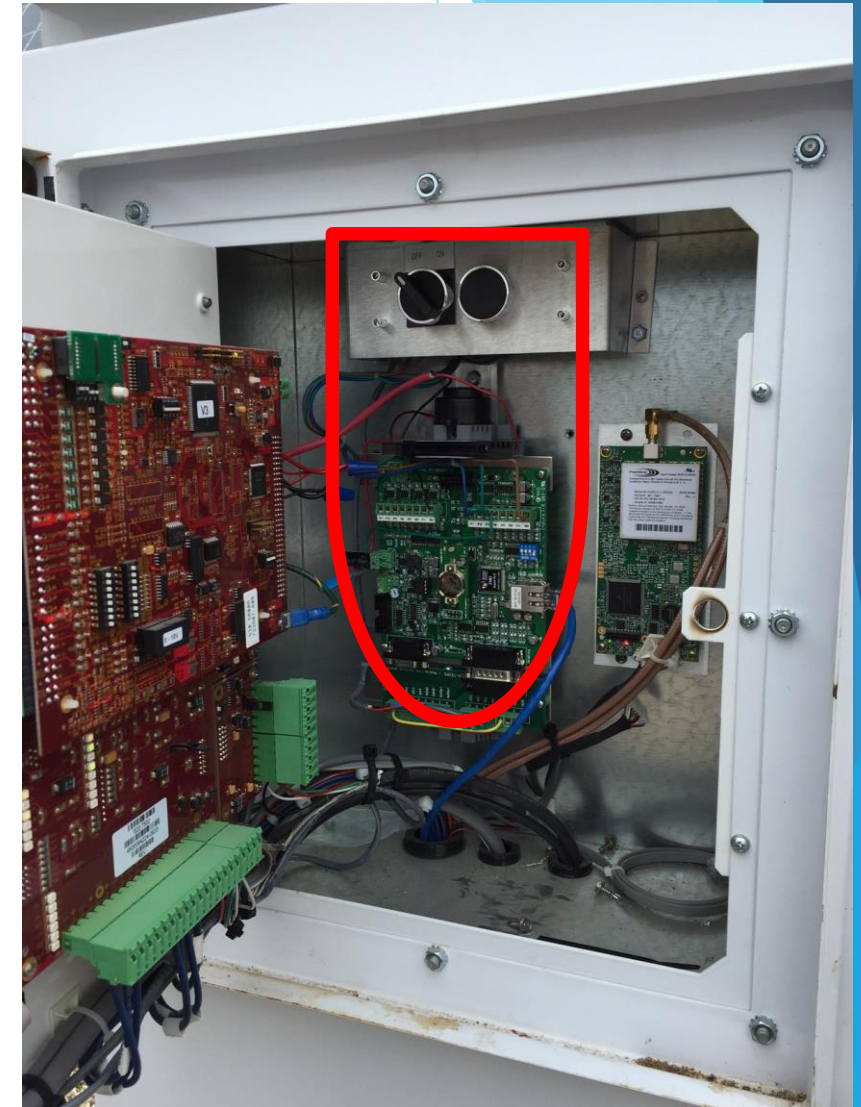
Factors Working Against PSO Adoption



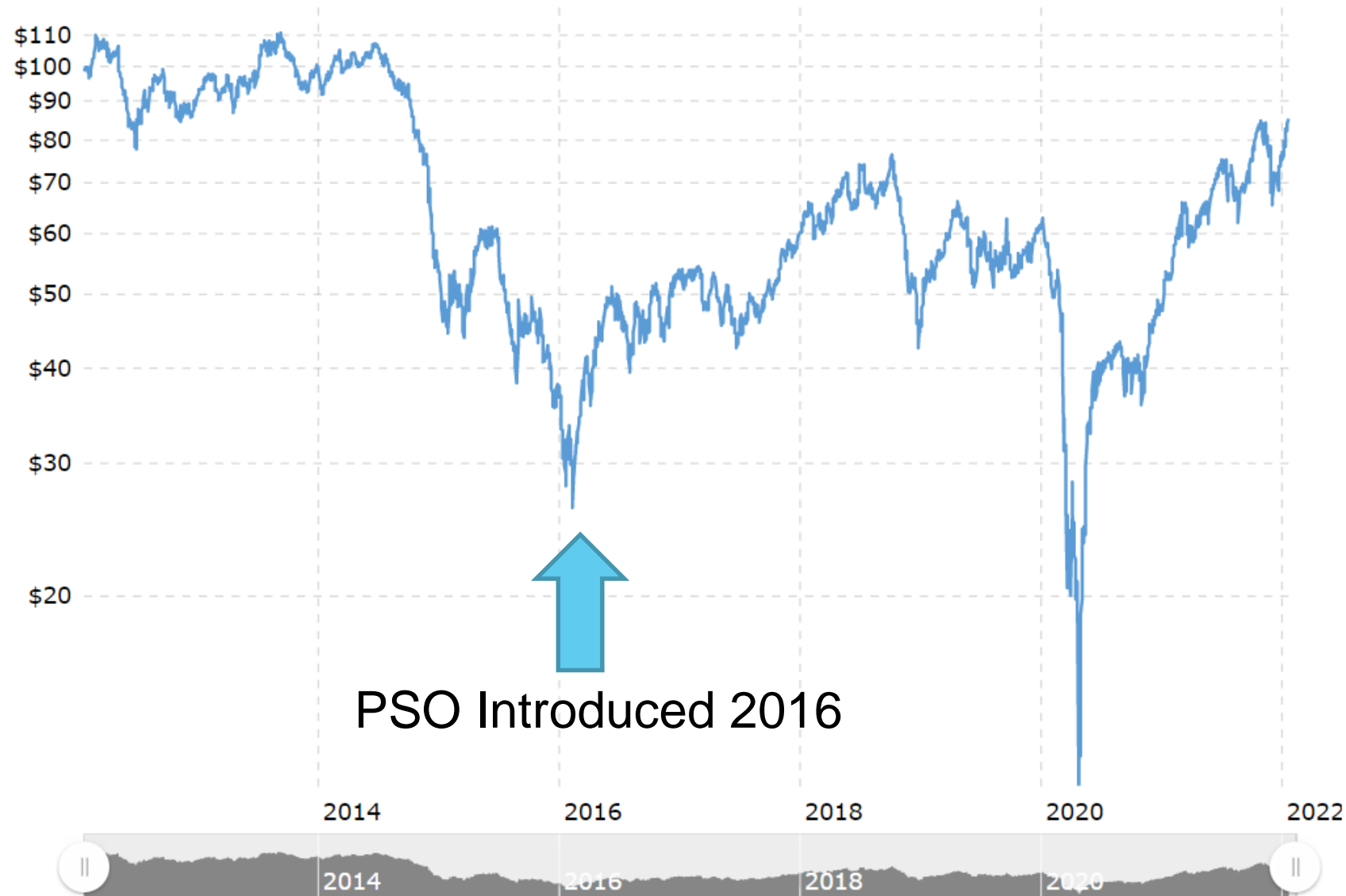
- ▶ SDSM / PSO doesn't increase production
 - ▶ Makes same production with less strokes (less wear)
 - ▶ Lower power consumption documented
 - ▶ Neither were home run reasons
- ▶ Could not prove that less strokes and higher minimum rod loads would result in less failures
 - ▶ No long-term failure studies performed
- ▶ Pumps with leaking standing valves lost production
 - ▶ 5% of pilot test wells saw this

Factors Working Against PSO Adoption

- ▶ Is major change in operation
 - ▶ Simulation programs can't handle it
 - ▶ Unrealized fears about equipment failures
 - ▶ Required PLC to be inserted in RPC cabinet
- ▶ RPC companies felt threatened
 - ▶ Wasn't invented by them
 - ▶ Hardware could not perform PSO Part 2
 - ▶ Encline had applied for a patent
 - ▶ Result: Warranty voided if operator tried
- ▶ Oil price dropped and spending stopped



Factors Working Against PSO Adoption



Factors Working Against PSO Adoption



- ▶ Gas Lift became popular for horizontals
 - ▶ Less industry interest in rod pumping
 - ▶ Introduction of HPGL in 2016 shifted Encline resources from PSO due to idea importance
- ▶ Slow Downstroke Mode and PSO are not plug and play
 - ▶ SDSM requires routine parameter review
 - ▶ PSO sets all parameters, but requires periodic algorithm evaluation
 - ▶ Neither simple enough for busy operator personnel
 - ▶ Opportunities for Machine Learning?



The Future?

- ▶ Encline dropped all patent efforts years ago when it became clear that adoption would be difficult
- ▶ RPC manufacturers are free to incorporate PSO
- ▶ Operators are free to incorporate PSO into Data Analytics / Machine Learning efforts
 - ▶ Let the cloud tell the RPC upstroke and downstroke pumping speeds



Acknowledgements/Thanks & Questions

Thanks to Lynn Rowlan, Jim Lea, and Jim McCoy for allowing use of their 2012 Pump Slippage slides in this presentation

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Thanks to all operators who performed trials of PSO and opted to support Encline's R&D efforts by purchasing PSO hardware



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